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Plot No.48A, 2nd Main Road,
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Pallikkaranai, Chennai - 600 100.
GST NO. 33AADCE6103A2ZH
PAN NO. AADCE6103A

Eco Tech Labs Pvt Ltd

Ph No : 044-35692477
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Website : www.ecotechlabs.in
CIN : U74900TN2014PTC094895

To

The Member Secretary,
Chennai Metropolitan Development Authority
Thalamuthu- Natarajan Building
No.1 Gandhi-Irwin Road
Egmore, Chennai -600008

Sir,

Sub: Concurrence for the design of proposed in-situ Sewage Treatment Plant of **110 KLD** for the Proposed Construction of Residential Development New Door No. 4/121, Goparasanallur main road, Kattupakkam, Chennai 600 056 comprised in Survey No. 84/1A, 85/1, 91/4B, 92/3, 91/3, 92/2, 83/1 & 84/2, situated at Goparasanallur Village, Poonamallee Taluk, Thiruvallur District – Reg.

With reference to above subject "CMWSSB had been issuing Concurrence for the design of sewage treatment plants. Based on the request from the project proponents in the 253rd Authority meeting of CMDA held on 21.07.2016, the Authority resolved that the NOC from CMWSSB for STP design clearance and Swimming pool need not be insisted either for issuing Planning Permission or Completion Certificate and the design sufficiency certificate issued by registered professionals/ institutions shall be accepted" based on the above reference letter the proponent has approached me for the design sufficiency certificate vide reference cited 1st above for their Sewage treatment plant of capacity of **110 KLD**.

I, Dr A. Dhamodharan – Environmental Specialist (Approved Water Pollution Expert by NABET –Quality council of India) &Managing Director of Eco Tech Labs Pvt Ltd, Registered Functional Area Expert as Water & wastewater Specialist by QCI NABET Govt India, for Building & construction projects (NABET certificate Number: NABET/ EIA/2124/ SA 0147) & Adjunct Faculty in Civil Engineering Department at R.M.K. Engineering College, R.S.M. Nagar, Kavaraipettai.

The design and drawings submitted by the proponent has been scrutinized for design feasibility as per CPHEEO norms, and suggestions and correction intimated to the proponent, and same has been corrected and submitted by the client for the STP capacity of **110 KLD**. The design adequacy calculation and drawings enclosed along with this letter with the following recommendations,

1. The capacity of STP **110 KLD – MBBR** – domestic determined by the proponent in scrutiny of design of proposed in situ STP.

2. The effluent characteristics for domestic sewage generated from the development and effluent characteristics in the effluent of STP as assumed and given by the applicant

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has been considered as basic data in scrutiny of the design of the in situ STP and is furnished below

Description	Influent characteristics	Effluent characteristics
pH	6.5 - 8	6.5 – 8
Total Suspended solids	450 mg/L	< 20
BOD at 27. C	350 mg/L	< 20
Oil & Grass	20 mg/L	< 10

3. The treatment units are proposed to be constructed below GL with access from Manhole opening provided at ground level. The panel board and air blowers are to be placed on the platform of STP. The air inflow pipe to blowers and air vent pipe to be laid below drive way and fixed in the compound wall for air circulations

4. The proponent ensured that the structures provided for the underground treatment units are waterproof. And also rain water entry in the site is insisted to be prevented to the STP tanks.

5. The treatment units are placed below the ground level and hence the sufficient air circulation through duct and also the methane gas detectors is recommended during operation phase to ensure the safety of operators

6. The treated water is proposed for gardening and flushing and hence the proper disinfection by UV is recommended during operation phase, routine check up for microbiological growth is recommended during operation phase.

7. The sludge generated in the STP is recommended to compost and reuse as gardening manure hence it is purely organic in nature.

With the above recommendations, I certify that the proposed STP design (Plan enclosed) is adequate to treat the sewage generated in the above residential complex, the attested drawings and design calculation in enclosed along with this letter. The concurrence certificate is issued based on the design submitted and standard design check done with reference to CPHEEO manual.

Thanking You,
Yours Sincerely,

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Managing Director
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STP DESIGN EVALUATION REPORT

For

110 KLD SEWAGE TREATMENT PLANT

To be Constructed for Residential building

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Technical Specification

Dr. A. C...
(NABET AP...
NA...
Eco ...
Plot No.48A, 2nd ...

Technical specification and design adequacy calculations

Design Basis

Design capacity	: 110 KLD
Operating Hours	: 24 hrs
Plant Flow Rate/Phase	: 4.58 m^3 / hr
Design Flow Rate	**: 4.58 m^3 / hr**

Quality logistics

S.No	Description	Unit	Inlet	Outlet	Standards
1	pH		7 - 8	7 – 7.5	6.5 – 8.5
2	TSS	mg/ l	200 – 250	<2	<30
3	BOD	mg/ l	350 – 400	<10	<20
4	COD	mg/ l	400 – 500	100	<250
5	Oil & Grease	mg/ l	30 – 45	Nil	<5

Process Description

The sewage generated from the various sources will be collected in the equalisation tank through the screen chamber to remove floating material and particle size greater than 20 mm. The Screened sewage is then led to the aeration tank through Raw Sewage Transfer Pump. Coarse bubble diffusers are provided in the collection tank.

In the aeration tank, air is diffused through special type of diffusers to oxidize the organic matters with the help of air blower & diffuser arrangement. Biological treatment takes place through MBBR media. The MBBR (Moving Bed Bio Reactor) media which introduced in to the aeration system at the rate of 80000 nos per cubic meter to increase the surface area of the aeration tank, the bacteria will fix in the rough surface the plastic media is submersible floating conditions will enhance the growth of microorganism and improve the BOD reduction in the aeration tank, Then the overflow from aeration tank is sent to the Clarisettler tank for settling. The bioflocs formed in the aeration tank will be settled at the bottom of the Clarisettler tank through Clarifier rake mechanism and the settled sludge will be pumped to the sludge holding

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tank through the return sludge pump. From sludge holding tank, the sludge will be fed to filter press unit for dewatering purpose through screw pumps.

The clarified overflow will be collected in the Clarified water tank where sodium hypo chlorite is given online with the help of dosing system for disinfection purpose. The disinfected water is then fed to the Pressure Sand Filter, Activated. Carbon Filter and Water Softener through Filter feed pump for the removal of suspended solids, organic matter, odour and salt of Calcium & magnesium (Hardness).

In this process MLSS concentration in aeration tank will be maintained between 3000 – 3500 mg/L. To maintain this concentration sludge from secondary clarifier will be recirculated to aeration tank. The microorganisms present in the sludge will digest the organic compounds present in the sewage and thus reduces BOD and COD content of the inlet sewage. Oxygen required for the survival of the microorganisms will be supplied through air blower and diffuser arrangements. The other pollutants will be reduced by various treatment steps as given above.

The treated water can be used for flushing & gardening purpose.

Components of STP

- Equalization tank
- Aeration tank with MBBR media
- Settling tank
- Filtration through Sand filter and Carbon Filter
- UV Disinfection
- Sludge Thickener/Disposal
- Ultra Filtration (Tertiary treatment)
- Treated sewage collection tank.

Bar Screening

Sewage generated from the development activity will flow by gravity into the bar Screen Chamber, where Bar Screen is fixed to arrest suspended trashy matter such as, paper, rags, vegetable wastes, leaves, cotton waste etc. The bar screens have to be cleaned manually using a hand rake and these screenings to be collected and disposed off at regular intervals to landfill.

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Equalization (Collection) Tank

Sewage free from trashy matters will be collected in the Equalization Tank by gravity. The tank acts as a holding tank for the raw effluents in order to homogenize the wastewater quality, control the dampening flow, constant feed water flow rate to rest of the treatment plant etc. To prevent odour and to improve the efficiency of oxidation process, oxygen will be supplied by means of diffusers and air blower.

Aeration tank with MBBR Media

Moving Bed Biofilm Reactor MBBR process is a state-of-the-art fixed-film (or attached growth) biological process used for wastewater treatment both municipally and industrially for BOD removal, nitrification and denitrification.

A Moving Bed Biofilm MBBR reactor consists of a tank with submerged but floating plastic (usually HDPE, polyethylene or polypropylene) media having specific gravity less than 1.0. The large surface area of the plastics provide abundant surface for bacterial growth. Biomass grows on the surface as a thin film whose thickness usually varies between 50-300 microns. Medium or coarse bubble diffusers uniformly placed at the bottom of the reactor maintains a dissolved oxygen (DO) concentration of > 2.5-3 mg/L for BOD removal. Higher DO concentrations are maintained for nitrification. To retain the media flowing out of the tank, screens are placed on the downstream walls. A clarifier or a DAF is placed downstream of the MBBR tank to separate the biomass and the solids from the wastewater. No sludge recycle is required for this process.

For denitrification, anoxic Moving Bed Biofilm Reactor MBBR tanks are used. The anoxic tank is similar to aerobic Moving Bed Biofilm Reactor MBBR tank described above except that no oxygen is supplied. The tank contains no diffusers and the media is kept in suspension in the reactor through submersible mixers. Other feature such as the screen is the same as aerobic reactor although the design may be slightly different.

A schematic of the Moving Bed Biofilm Reactor MBBR process for BOD removal and/or nitrification is shown. Wastewater enters the Moving Bed Biofilm Reactor MBBR where the biomass attached to the surface of the media degrades organic matter resulting in BOD removal and/or nitrification depending on the type and characteristic of the wastewater. Organic carbon is converted to carbon dioxide and leaves the system while the ammonia and nitrogen in the organics are converted to nitrates through nitrification process. Oxygen required for the

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process is provided through the diffusers installed at the bottom of the reactor. The treated wastewater then flows through the screens to the downstream clarifier/DAF where the biomass and solids are separated from the wastewater.

In the aeration tank, air is diffused through special type of diffusers to oxidize the organic matters with the help of air blower & diffuser arrangement. Biological treatment takes place through MBBR media. Then the overflow from aeration tank is sent to the Clarisettler tank for settling. The bioflocs formed in the aeration tank will be settled at the bottom of the Clarisettler tank through Clarifier rake mechanism and the settled sludge will be pumped to the sludge holding tank through the return sludge pump. From sludge holding tank, the sludge will be fed to filter press unit for dewatering purpose through screw pumps.

Aeration tank is the major Reaction tank for the biological process. Aeration tank is provided with diffused aeration / mixing system, where in tubular membrane diffuser or medium bubble diffuser are arranged at the bottom of the tank and air is fed with air blowers. Aeration process will be taking place for 24 hours continuously. The waste water in the aeration tank utilize the oxygen fed through air blowers and the micro organism (Bio-Mass) starts growing using the nutrients (Organic compounds) present in waste water. The contents of the aeration tank are called "Mixed liquor and suspended solids as mixed liquor suspended solids". (MLSS), which is in fact the active Bio–mass responsible for bio-degradation of the effluent. The Bio-mass comprises chiefly of bacteria and to some extent lower form animals such as rotifiers and protozoa.

Secondary Clarifier / Settling

The overflow from aeration tank is led into the secondary clarifier tank by gravity. It is provided with bottom scraper arm (in some cases this is not provided) which rotates slowly by means of a central drive arrangement. The sludge which settles at the bottom is scrapped and is directed towards the sludge well at the center. The sludge collected at the center is pumped to aeration tank and to sludge sumps by sludge pumps. The clarified sludge scraping mechanism to be operated continuously as long as there is raw waste water inflow in to the aeration tank.

Sludge Disposal

Sludge will be recirculated to aeration tank for carry out extended aeration process from secondary clarifier. The excess sludge will be collected in a separate sump and then feed into a

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filter press arrangement where the sludge will be thickened. The thickened sludge will be removed from the filter cloths manually and should be dried and used as manure for gardening. The supernatant solution from filter press will be again sent to collection tank for treatment.

Treated water Storage Tank

The clear water overflowing from the secondary clarifier is collected in a tank called clarified water sump. This water is generally have desired characteristics required for water to be used on irrigation land with 92-95% of BOD5 removed.

Pressure Sand Filter (PSF)

The treated effluent from the sump is pumped to Multigrade sand filter where further reduction in TSS, BOD_5, odour and color will takes place. This is a pressure vessel equipped with a perforated under drain plate. Here the sewage will filtered with polystyrene strainers filled with filter media comprising of graded gravel, sand and pebbles. The suspended particulates are arrested and the clean filtered water coming out from the Multigrade sand filter is led to Activated carbon filter for further treatment.

Activated Carbon Filter (ACF)

The filter water from the Multigrade sand filter passes through the activated carbon filter, which is also a vertical pressure vessel. It is also equipped with perforated plate with polystyrene strainers at the bottom and top perforated brass strainers. In between is the filter media comprising of 900-1000 mm activated carbon granules over a bed of graded gravel.

In ACF any odour and to certain extent colour in the waste water is absorbed by the carbon and the filter water is absolutely sparklingly clear.

Ultra filtration

The treated wastewater from the filters will be then passed to ultra filtration for complete reduction of Total suspended solids, microbes and color of the water, since the wastewater is utilized for the flushing purposes it the residential apartment, we need the treated water quality in Nil TSS and BOD less than 10 mg/l.

The STP treated water is pumped to Bag Filter for finer filtration and it is taken to the UF membrane where high molecular weight substances, colloidal materials, and organic and inorganic polymeric molecules are removed. The Product Water is taken to Product water Storage tank and Reject is led into drain.

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The UF system comprises of UF membranes housed in FRP pressure tube. All interconnecting pipe lines in UPVC & Pneumatic Hoses. Necessary instrumentation is provided to monitor the operation of the system.

Almost all components/equipments of the UF unit will be pre-engineered, pre-wired, pre-tested and ready for use after giving necessary interconnections. The UF block will be totally skid mounted. Each unit will be a product of high quality workmanship, skilled and experienced mechanical design.

Adequacy Evaluation of the Sewage Treatment Plant of 110 KLD

SPECIFICATION OF EQUALISATION TANK

Adequacy Calculation

Volume of the Equalisation Tank, V : 46 m^3

Flow Rate, Q : 4.5 m^3/hr

Retention Time : 46/4.5

: 10 hours

Standard Retention hours for Equalisation Tank is 8-12 hrs

Provided Retention hours is = or > standard retention hours.

Hence it is adequate

SPECIFICATION OF AERATION TANK

Adequacy Calculation

Volume of the Aeration Tank, V : 55 m^3

Flow Rate, Q : 4.5 m^3/hr

Retention Time : 55/4.5

: 12 hours

Provided retention hours is = or > standard retention hours.

Hence it is adequate

SPECIFICATION OF SECONDARY SETTLING TANK

Adequacy Calculation

Volume of the Secondary Settling Tank, V :19 m^3

Flow Rate, Q : 4.5 m^3/hr

Retention Time : 19/4.5

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: 4 hours

Standard Retention hours for Secondary Settling Tank is 4 – 6 hrs

Provided retention hours is = or > standard retention hours.

Hence it is adequate

SPECIFICATION OF CLARIFIED WATER TANK

Adequacy Calculation

Volume of the Clarified water Tank, V : 46 m^3

Flow Rate, Q : 4.5 m^3/hr

Retention Time : 46/4.5

: 10 hours

Standard Retention hours for Clarified water Tank is 4 – 6 hrs

Provided retention hours is = or > standard retention hours.

Hence it is adequate

SPECIFICATION OF SLUDGE HOLDING TANK

Adequacy Calculation

Volume of the sludge holding Tank, V : 8 m^3

Flow Rate, Q :4.5 m^3/hr

Retention Time : 8/4.5

: 1.7 hours

Provided retention hours is = or > standard retention hours.

Hence it is adequate

SPECIFICATION OF AIR BLOWER

Adequacy Calculation

Assume O_2 requirement : 2.5 kg of O_2/ 1kg of BOD

: 1 kg of BOD / 2.5 kg of O_2

Assume BOD for sewage : 300 mg/l = 0.3kg / m^3

BOD Load : 110 x 0.3 = 33 kg of BOD / day

O_2 requirement : 33 x 2.5 =82.5 kg of O_2 / day

Oxygen transfer @ 16% of SOTR : 82.5 / (0.16 x 0.23 x 0.65 x 0.95)

: 82.5 / 0.022 = 3634

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$\alpha = 0.65$; $\beta = 0.95$; Density = 1.16

= 3634/ 1.16 = 3132 m^3/ day

Air requirement = 3132/ 24 = 130 m^3/ hr

Hence air flow rate is adequate

SPECIFICATION OF PRESSURE SAND FILTER

Adequacy Calculation

Flow rate Q : 4.5 m^3 / hr

Considering the operation of 16 hours of filter

Filtration rate for PSF (V) : 8 m^3 / m^2 hr

Q : A x V

A : 4.5/8

: 0.5625 m^2

D^2 : 0.5625 x 4 / 3.14

: 0.716

D : 0.84 m

Diameter provided: 1000 mm

Hence adequate

SPECIFICATION OF ACTIVATED CARBON FILTER

Adequacy Calculation

Flow rate Q : 4.5 m^3 / hr

Considering the operation of 16 hours of filter

Filtration rate for ACF (V) : 8 m^3 / m^2 hr

Q : A x V

A : 4.5/8

: 0.5625 m^2

D^2 : 0.5625 x 4 / 3.14

: 0.716

D : 0.84 m

Diameter provided: 1000 mm

Hence adequate

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SPECIFICATION OF FINAL TREATED WATER TANK

Adequacy Calculation

Volume of the Final Treated Water Tank, V: 55 m^3

Flow Rate, Q : 4.5 m^3/hr

Retention Time : 55/4.5

: 12 hours

Hence it is adequate

SPECIFICATION OF UF TREATED WATER TANK

Adequacy Calculation

Volume of the UF Treated Water Tank, V: 27 m^3

Flow Rate, Q : 4.5 m^3/hr

Retention Time : 27/4.5

: 6 hours

Hence it is adequate

CONCLUSION AND RECOMMENDATIONS

Considering the following as the influent sewage load,

Suspended solids - 150-200 mg/L

BOD - 300-350 mg/L

The final BOD of the treated wastewater from the proposed sewage treatment plant will be below 10 mg/L and the suspended solids concentration will be below 30 mg/L based on the above evaluation.

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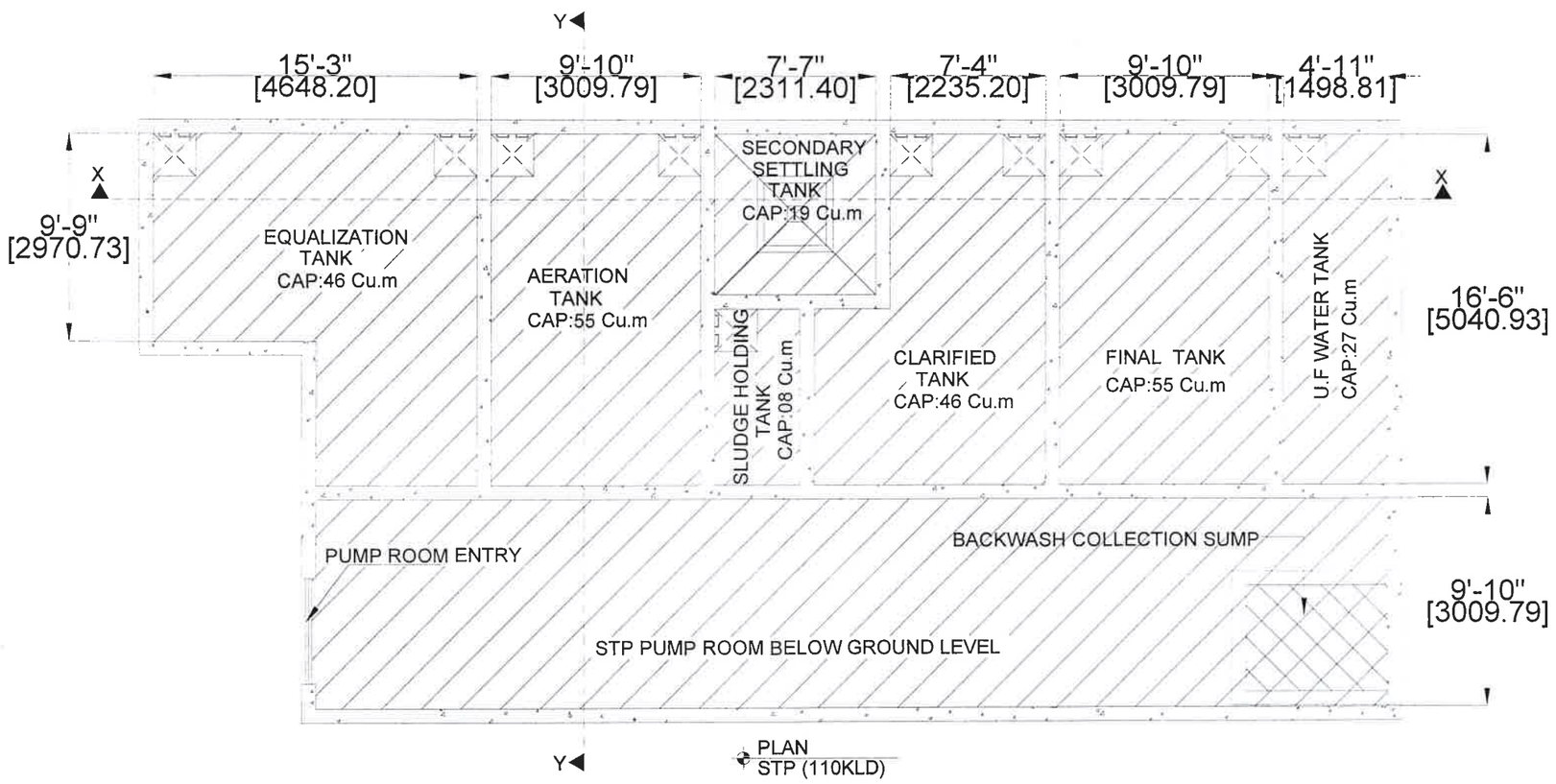
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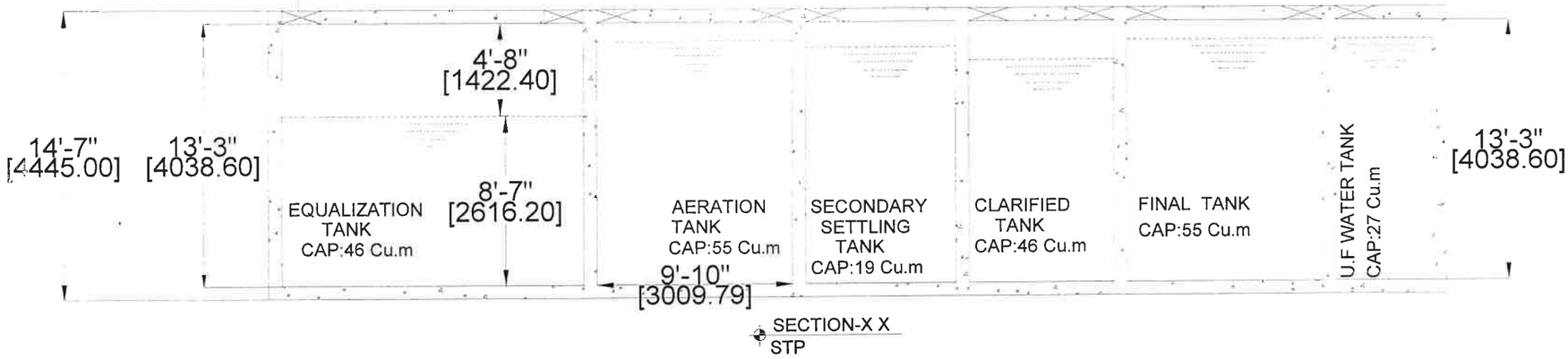
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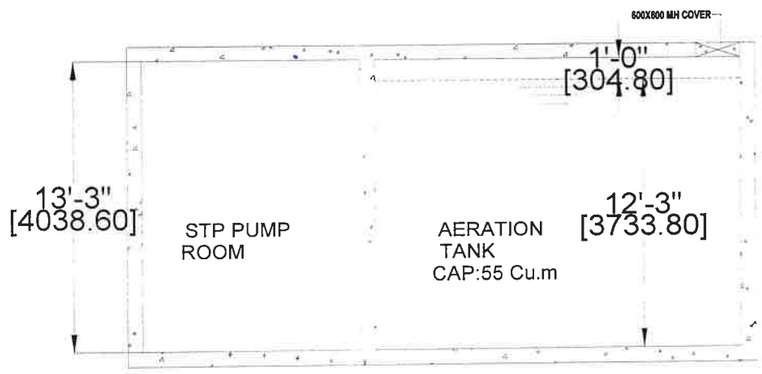
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**********End of report **********

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